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# Research

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Uranium Aerosol Characteristics at a Nuclear Fuel Manufacturing Site - Particle Size, Morphology and Chemical Composition

#### SSM perspective

#### Background

All nuclear facilities require that working areas are controlled and measured regarding external radiation and surface- and air contamination.

The different methods used to calculate the committed effective dose caused by continuous intake via inhalation are associated with large uncertainties. Material characteristics determine how the airborne radioactivity (in case of this project; uranium aerosols) are trapped in the nose, trachea and lungs and then dissolve in body fluids, such as lung fluid. A certain part of the aerosols ends up in the nasal mucus and follows the intake path through the digestive tract and out into the blood.

Small particles behave differently than large particles when inhaled. Small particles (< 2 micron AMAD, Activity Median Aerodynamic Diameter) have a stronger tendency to reach deep into the lungs (alveoli) than large particles. The respiratory system can easier get rid of larger particles. However, it is not only the particle size distribution that is important but also how the activity is distributed between these particle sizes.

There is a need for better knowledge of material- and aerosol characteristics of airborne radioactivity present in the work environment in the operation of nuclear facilities.

#### Objective

The project will perform a pre-study about how the uranium aerosols can be characterized in the aspect of size, appearance, and in formations with other particles. At the nuclear fuel factory in Västerås operational situations occur resulting in production of airborne uranium particles (uranium aerosols) that the project will use in the research study by collecting these aerosols with various type of filters. Linköping University will be the project manager of the research project. This research is expected to describe the characteristics in terms of size and activity distribution and internal structure of the uranium aerosols from the different process steps in a nuclear fuel factory.

The study will provide more knowledge of the importance of monitoring air and surface contamination. Since the calculations of the committed effective dose caused by continuous intake via inhalation are associated with large uncertainties the authority initiated this pre-study to be performed.

#### Summary by the authors

The main conclusions of this project pre-study are:

- Uranium aerosols vary significantly with respect to size and shape. There are indications of different 'families' of particles with respect to size distribution.
- Uranium aerosols are generally observed as discrete particles, but large conglomerates of loosely attached uranium particles were also observed.

• Uranium aerosols can consist of mixtures of uranium oxides, fluorides, nitrites and gadolinium. The aerosols are frequently attached to other elements such as aluminum and silicon in the shape of either discrete particles or other materials.

#### Need for further research

Being a pre-study, one aim of the present work was to identify prioritized future studies, including:

- Estimating particle volumes, activities and correlation to the aero dynamic diameter in order to estimate the influence on AMAD calculations,
- Carrying out complete sampling using 8-stage impactors,
- Carrying out radiometric analysis of all impactor stages,
- Additional chemical form analysis, e.g. AUC quantification,  $UO_2/U_3O_8$  ratios, U-F chemical form, and,
- Solubility experiments.

#### **Project information**

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# **2015:18** Uranium Aerosol Characteristics at a Nuclear Fuel Manufacturing Site - Particle Size, Morphology and Chemical Composition

This report concerns a study which has been conducted for the Swedish Radiation Safety Authority, SSM. The conclusions and viewpoints presented in the report are those of the author/authors and do not necessarily coincide with those of the SSM.

# Sammanfattning

Vid alla kärntekniska verksamheter krävs att strålningsmiljön kontrolleras dels genom mätningar av ytors- och luftens kontamination i anläggningen och dels med persondosimetriverksamhet inkluderat helkroppsmätning.

De olika metoder som används för att beräkna intecknad effektiv stråldos från kontinuerligt intag via inandning är förknippade med stora osäkerheter.

Materialkarakteristiken är avgörande för hur den luftburna aktiviteten (i projektets fall uranaerosoler) fastnar i näsa, luftstrupe och sedan lungorna och löses upp i kroppens vätskor, t.ex. lungvätskan. En viss del av aerosolerna hamnar i näsans slem och följer intagsvägen via mag- tarmkanalen och vidare ut i blodet.

Små partiklar (< 2 µm AMAD) som inhaleras uppför sig annorlunda än stora partiklar. De har bl.a. större förmåga att tränga ner djupare i lungorna och nå alveolerna. Luftvägarna har i allmänhet lättare att göra sig av med större partiklar, som då snabbare kan lämna kroppen. Det är emellertid inte endast partikelstorleksfördelningen som är av betydelse, utan även hur aktiviteten fördelas mellan dessa storlekar.

Det finns ett behov av bättre kunskap om material- och aerosol karakteristik för luftburen radioaktivitet som finns i verksamheten vid kärntekniska anläggningar. Därför ska detta forskningsprojekt utreda hur uranaerosoler kan karakteriseras med avseende på bl.a. storlek, utseende och hur dessa sammanhålls i formationer med andra partiklar. Vid Bränslefabriken i Västerås tillverkas kärnbränsle och i verksamheten förekommer luftburna uranpartiklar s.k. uranaerosoler som projektet använt för forskningsstudien genom att samla in dessa med hjälp av olika filter. Linköpings universitet utförde som myndighetsstöd denna förstudie i ett forskningsprojekt. Målet är att kunna redogöra för uranaerosolers karakteristik med avseende på storleksoch aktivitetsfördelning, samt inre struktur hos uranpartiklar från olika processteg i en kärnbränslefabrik.

Resultaten visar på att uranaerosoler i studien varierar signifikant med avseende på storleksdistributionen. I förstudien observerades uranaerosoler allmänt som diskreta partiklar, men även i förekomster med andra partiklar löst fästa i varandra. Uranaerosolerna förekommer även i olika former av uranoxider.

Vidare studier som projektet identifierat är bl.a. att utreda hur uranaerosolers partikelvolymer i förhållande till deras aerodynamiska diameter påverkar AMAD beräkningar. Vidare behövs fler antal luftprover genomföras och analyseras. Ytterligare moment att utreda är uranaerosolers kemiska form och förhållanden som t.ex. löslighet.

# Uranium Aerosol Characteristics at a Nuclear Fuel Manufacturing Site -Particle Size, Morphology and Chemical Composition

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#### Abstract

Knowledge of radioactive aerosol characteristics is crucial in order to carry out accurate internal dosimetry calculations following the International Commission on Radiological Protection methodology. Examples of such parameters are Activity Median Aerodynamic Diameter and solubility. Understanding of such parameters requires knowledge of aerosol characteristics such as size distribution, morphology and chemical form.

In this pre-study, these parameters have been studied at two process steps (fluidizing bed furnace and burnable absorber grinder) at the Westinghouse Electric Sweden AB nuclear fuel factory in Västerås, Sweden. Aerosols were collected using a cascade impactor and analyzed with Scanning Electron Microscopy coupled with Energy Dispersive X-ray analysis.

The results show a significant variation in uranium aerosol shape (spherical, nearcylindrical, irregular with sharp edges, conglomerates of small particles, etc.), with particle size distributions to some extent deviating from the expected lognormal distribution, possibly indicating two 'families' of particles.

The vast majority of the radioactive aerosols consist of uranium and oxygen, but at the bed furnace, 1-6 % of the uranium aerosols contained fluorine. Other uranium aerosols were attached to/consisted of elements such as nitrogen, aluminum, gado-linium and silicon.

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## Abbreviations

AMAD	Activity Median Aerodynamic Diameter
AMTD	Activity Median Thermodynamic Diameter
BS	Backscatter
CRP	Coordinated Research Project
EDX	Energy Dispersive X-ray
IAEA	International Atomic Energy Agency
ICRP	International Commission on Radiological Protection
LiU	Linköping University
MCE	Mixed Cellulose
SEM	Scanning Electron Microscopy
SDD	Silicon Drift Detector
WSE	Westinghouse Electric Sweden AB

### Introduction

Nuclear fuel manufacturing sites handle large amounts of uranium in various chemical forms. Uranium, consisting of isotopes being alpha emitters, requires careful monitoring of internal contamination among workers. This can be carried out in different ways, one being urine sampling and analysis in order to evaluate chronic or acute intake.

Internal dose calculations based on urine sampling require knowledge about the material characteristics in question (ICRP 1994). In particular, the particle Activity Median Aerodynamic Diameter (AMAD) and aerosol solubility need to be investigated. The present work is a pre-study of uranium aerosol size distribution, morphology and chemical composition at the Westinghouse Electric Sweden (WSE) nuclear fuel factory in Västerås, Sweden.

The International Commission on Radiological Protection (ICRP) has suggested that an AMAD of 5  $\mu$ m should be used in absence of site specific information (ICRP 1997). The 5  $\mu$ m figure has previously been validated throughout the literature, primarily by using cascade impactors. For example, Kravchik et al. (2008) presented AMAD measurements ranging between 1.6-11.0  $\mu$ m at an uranium processing plant. Thind (1987) and Ansoborlo (1989) presented AMAD values for different work locations ranging between 4-10  $\mu$ m. All studies were in fair agreement with the suggested 5  $\mu$ m ICRP value.

Furthermore, review articles exist on the matter, and some summarize AMAD measurements carried out at nuclear fuel factories (Connelly and Jackson, 2013; Dorrian and Bailey, 1995). The presented AMADs showed some significant variation, e.g. pellet press measurements ranged between 3.9-8.8 μm and uranyl fluoride between 1-9 μm. Exact sampling locations were not always specified. While information about uranium particle morphology exists (IAEA, 2011), publications specialized towards aerosol characteristics are scarcer (Ansoborlo, 1997; Eidson, 1980). The need for increased knowledge about radioactive particles has been identified by the International Atomic Energy Agency (IAEA). A coordinated research project (CRP), *"Environmental Behaviour and Potential Biological Impact of Radioactive Particles"* has been initiated. Results from this study will be presented within this CRP.

The WSE factory operates a wet chemical process where  $UF_6$  is converted via ammonium uranyl carbonate (AUC) to  $UO_2$ . The  $UO_2$  is pelletized by pressing, sintering, grinding and finally inspected before insertion into fuel rods. In addition, there is a burnable absorber (BA) pelletizing workshop, as well as a large number of side processes, allowing for recycling of uranium production waste. Most process steps mentioned in this work have, to the best of the author's knowledge, not been covered in the literature with respect to AMADs or particle morphology.

The aerosol shape is indirectly considered in AMAD estimates when cascade impactors are used. Aerosol size separation is achieved based on the particle's aerodynamic properties, where particle shape, described by the shape factor (Hinds, 1999) plays an important role, see Equation 1,

$$d_a = d_e \sqrt{\frac{p_p}{p_0 \chi}} \tag{1}$$

where,

 $d_a$  (µm) is the aerodynamic diameter,

 $d_e$  (µm) is the irregular particle's equivalent diameter,

 $p_p$  is the standard particle density (1000 kg/m<sup>3</sup>),

 $p_0$  (kg/m<sup>3</sup>) is the irregular particle density and

 $\chi$  is the shape factor (no unit). The shape factor is unity for a sphere, 1.08 for a cube, 1.32 for a cylinder (lying down) with a length four times the diameter. A conglomerate of two spheres has a shape factor of 1.12 (Akselsson et al. 1994).

Particle shape affects resuspension, where rough (uneven) particles are subject to a weaker adhesive force to a surface compared to smooth particles (Qian et al., 2014). Resuspension from surface contamination plays a major role in worker exposure. Hence knowledge on particle shape is of interest in everyday radiation protection work.

In this pre-study, four sites were selected for cascade impactor sampling and scanning electron microscopy (SEM) coupled with energy dispersive X-ray (EDX) measurements. The purpose of the pilot-study was to provide preliminary information on uranium aerosol characteristics at a nuclear fuel factory, in order to later on carry out a complete survey based on findings and learning experiences.

### **Uranium Aerosol Collection**

#### **Collection sites**

Uranium aerosols were collected at four sites within the factory using a cascade impactor. Cascade impactors carry out aerosol separation based on particle inertia. Air is pumped through the impactor, which is divided into several stages. At each stage there is a filter medium, and air flow velocity is increased at each stage throughout the impactor. The inertia of large particles will cause them to impact onto filter media at the early stages of the impactor, whereas small particles require a higher velocity in order to impact onto filter media. Hence an aerosol separation based on particle aerodynamic diameter is accomplished.

The sites chosen were expected to generate a variety of particles with respect to AMAD, morphology and chemical composition. Sampling-related data are summarized in Table 1.

	Airflow through impactor (l/min)	Volume of air (m <sup>3</sup> )		
Site 1, Fluidized Bed	(a) 7.27 ± 2%	10.69		
Furnace	(b) 7.26 ± 1%	10.72		
Site 2, Grinder	8.01 ± 4%	10.78		
Site 3, Milling room	6.83 ± 7%	2.05		
Site 4, BA grinder	7.34 ± 1%	1.24		

Table 1: Impactor airflow and total air volume at the four sampling sites.

Site 1: The impactor was placed in a room above three fluidized bed furnaces where Ammonium-Uranyl-Carbonate (AUC) is led into three different furnaces, oxidizing AUC into  $UO_2$ . Hence, the airborne contamination in the room was expected to consist of a mixture of AUC,  $UO_2$  and  $U_3O_8$ . Sampling was carried out twice, one with MCE filters (a) and one with carbon tape (b).

Site 2: The impactor was placed in a milling room, where  $UO_2$  is milled as a preparation step for BA pellet manufacturing, which requires a finer powder for blending with gadolinium and pore building material. An AMAD smaller than the ICRP default value of 5  $\mu$ m was expected, with irregularly shaped particles dominating the morphology.

*Site 3:* The impactor was placed at one of the four pellet grinding stations in the pellet manufacturing workshop. At this station pellets are ground in order to obtain a specific diameter. An AMAD near the ICRP default value of 5 µm was expected (Thind, 1987), with irregularly shaped particles dominating the morphology.

Site 4: The impactor was placed at the pellet grinding station in the burnable absorber pellet manufacturing workshop. The operations are similar to those at *Site* 3, but the material differs since gadolinium and pore building material has been added. An AMAD smaller than the ICRP default value of 5  $\mu$ m was expected since a finer uranium powder is used. Particle morphology was expected to be similar to *Site 3*.

#### **Cascade Impactor and Filters**

A four-stage Sioutas Cascade Impactor was used with a Leland Legacy Sample Pump (SKC Cat. No. 100-3002). A four-stage impactor is not ideal for AMAD estimates due to the limited number of filter stages, giving rather poor size resolution. It is, however, suitable for SEM/EDX analysis, where filter analysis is very time consuming. Figure 1 shows the impactor used in the study as well as particles impacted onto a mixed cellulose (MCE) filter.



Figure 1: (a) The Sioutas Leland Legacy impactor and (b) Particles impacted onto a MCE filter casing the black strip ( $22 \times 1 \text{ mm}^2$ ).

The impaction cutoff is defined as the limit at which 50 % of all particles with a given aerodynamic diameter will impact onto the impaction medium. Adjusted cutoffs due to different flow rates are presented in Table 2.

The cutoffs were specified for a pumping flow rate of 9 l/min. Before and after each sampling session the flow rate was checked using an Alicat MB-50 SLPM-D flow meter. It was found that the pump was not always capable of maintaining a steady flow rate of 9 l/min. The flow rate was, however, nearly constant at 7.5 l/min. The pump was therefore set to a flow rate of 7.50 l/min, and cutoffs were adjusted (see Table 2) using Equation 2 (Copley and McDonald, 2009),

$$\frac{D_{50,2}}{D_{50,1}} = \sqrt{\frac{Q_1}{Q_2}} \tag{2}$$

where,

 $D_{50,2}/D_{50,1}$  is cutoff ratio correction factor,  $Q_1$  is the specified flow rate (l/min) and  $Q_2$  is the actual flow rate (l/min).

 Table 2: Cutoffs for the Sioutas Cascade Impactor as specified by the manufacturer at 9 l/min as well as adjusted cutoffs at different sampling sites.

Impactor	Specified	Adjusted cutoff (µm)					
stage	cutoff (µm) at 9 l/min	Site 1 (a)	Site 1 (b)	Site 2	Site 3	Site 4	
А	2.5	2.8	2.8	2.9	2.6	2.8	
В	1.0	1.1	1.1	1.1	1.1	1.1	
С	0.50	0.6	0.6	0.6	0.5	0.6	
D	0.25	0.3	0.3	0.3	0.3	0.3	

Different filters were available for the cascade impactor. MCE, pore size  $0.45 \,\mu\text{m}$  (SKC cat. No. 225-1911) were chosen for the four impaction stages and a glass fiber filter (Whatman GF/A, cat. Nr. 1820047) for the final collection filter. Glass fiber filters were chosen to obtain low pressure drop in the impactor (i.e. allowing high flow rates).

For *Site 1*, Bed furnace, additional sampling was carried out using sticky carbon tape instead of MCE filters on the impaction plates. The carbon tape's conducting properties was required in order to obtain high resolution images of small particles (<1  $\mu$ m) from the SEM-EDX analysis.

All filters were weighed before and after sampling, but the weight difference was insignificant. The impactor was decontaminated using isopropanol tissues before each sampling session in order to minimize the risk of filter cross-contamination.

#### **SEM-EDX** Analysis

All SEM-EDX analyses were carried out using a Carl Zeiss Microscopy Ltd EVO LS 15 Scanning Electron Microscope situated in IAEAs Environmental Laboratories (EL). The X-ray detector used for the Energy Dispersive X-ray (EDX) analysis was an electrical cooled 50 mm<sup>2</sup> Silicon Drift Detector (SSD) Oxford Instruments X-Max with an energy resolution of 125 eV of Mn K<sub> $\alpha$ </sub>-line. The software used for SEM-imaging was SmartSEM (version 5.06) and for the EDX analysis, INCA (version 5.03). Usually, 20 kV accelerating voltages were used in the EDX analysis enabling excitation of both uranium L and M electrons. Imaging was usually conducted in backscatter mode (BS). For the set using MCE filters, the analysis were carried out in variable pressure mode to minimize charging effects on the sample. The INCA software used a cobalt sample for calibration of the EDX system.

Since the area of impaction held tens of thousands of particles, the entire area could not be analyzed. Random fields were used, and scanning was run until 500-1000 uranium particles had been detected and analyzed on each impactor stage. The particle discrimination level was set to a particle length of 0.10  $\mu$ m.

Two sets of impactor filters (Stage A-D) were analyzed using SEM/EDX controlled by the particle software INCA: *Site 1, Bed furnace and Site 4, BA grinder*. Impaction material was carbon tape and MCE filters, respectively. The final filters (glass fibre) were not examined due to limited time for analysis.

Due to the irregular shape of many analyzed particles, the length parameter given by INCA has limited use for evaluation of particle size distribution. Instead, an adjusted particle diameter was calculated by transforming particle transectional area into a corresponding circular particle diameter. The overall particle size distribution (all impactor stages) was determined by random sampling and replacement of particles from each impactor stage. The number of sampled particles from each impactor stage was proportional to mean particle density (Table 3, Table 4).

Particle size distributions generally follow a log-normal distribution (Axelsson, 1994). This was evaluated by manually fitting a normal distribution to the logarithm of the particle length distribution.

## **Results**

This is a pre-study, and all results should be viewed as preliminary.

#### **Particle distributions**

A total of 3768 and 9177 particles from *Site* 1, Bed furnace and *Site* 4, BA-grinder, respectively, were analyzed. Table 3 and Table 4 show the number of particles detected per scanned field (field area: 7870  $\mu$ m<sup>2</sup>) for *Site* 1, Bed furnace and *Site* 4, BA grinder. The number of particles per field is not comparable for the two sites due to different sampling times and scan times.

Table 3: Mean number of detected particles per scanned field at Site 1, Bed furnace

	UO and/or AUC particles	UF particles	UF to UO/AUC-ratio
Stage A	50.7	3.1	0.06
Stage B	79.7	1.4	0.02
Stage C	43.9	0.6	0.01
Stage D	20.1	0.3	0.02

 Table 4: Mean number of detected particles per scanned field at the grinding station at Site 4, BA-grinder

	UO	UO with Gd	UF	UO with Gd to UO-
				ratio
Stage A	15.9	0.5	0	0.030
Stage B	23.7	0.5	0	0.020
Stage C	56.7	0.1	0.1	0.002
Stage D	45.0	0.1	0	0.002

Figure 2 shows the particle size distribution for impactor Stage A-D for *Site 1* and *Site 4*, as well as the overall particle size distribution (all stages). Figure 3 shows two examples (one poor fit, and one good fit) of how the log-transformed particle size distribution fits to a normal distribution. Table 5 shows particle size statistics.







**Figure 3:** Log-transformed particle diameter distribution for (a) all particles at *Site 1*, Bed furnace and (b) impactor stage C at *Site 4*, BA grinder. Super imposed are fitted normal distributions (red lines).

Table 5: UO particle statistics.

	Stage	Min (µm)	1:st quantile (µm)	Median (µm)	3:rd quantile (µm)	Max (µm)
	А	0.13	0.74	2.23	3.16	8.89
	В	0.13	0.86	1.30	1.74	5.91
Bed furnace	С	0.13	0.44	0.65	0.94	12.26
	D	0.13	0.24	0.34	0.50	3.60
	All	0.13	0.48	1.05	1.89	12.26
	А	0.13	0.40	0.70	1.35	18.70
	В	0.13	0.44	0.67	0.90	3.31
BA grinder	С	0.13	0.40	0.55	0.71	3.46
	D	0.13	0.25	0.35	0.47	3.64
	All	0.13	0.33	0.49	0.71	18.70

#### **Particle spectra**

Figure 4 shows examples of EDX spectra of uranium aerosols.



**Figure 4:** (a) Spectrum comparison of a UO (red line) and an AUC (yellow spectrum) particle. Notice the 0.392 keV K<sub>a</sub>-peak of N. (b) shows the spectrum of a UO<sub>2</sub>/U<sub>3</sub>O<sub>8</sub>-particle with Gd attached to it. Note the different energy scale of the spectra.

#### Particle size, shape and chemical form

A wide variety of uranium particle sizes and shapes were observed. The average uranium aerosol size was smaller at *Site 4*, BA grinder. Shapes ranged from spherical, pointy, irregular, cluster structures and combinations with other elements such as Al and Si.

Figure 5 shows a backscattered SEM image where high Z elements give a higher signal and shows as white spots in the image. This image gives an example of particle size variation and cluster structures at *Site 4*, BA grinding station. All white spots

in the image correspond to particles containing U and O. A few Gd-particles were found attached to the largest cluster.



**Figure 5:** Example of particle deposition showing particle size variation and particle clusters at *Site 4*, BA-grinding station. Image taken from impactor stage A in backscattered mode.

Figure 6 shows examples of uranium aerosol size and shape at *Site 1*, Bed furnace. For this particular image, an X-ray mapping was carried out for U (yellow) and N (red) using an accelerating voltage of 20 kV. Notice how the distribution of N does not always match the distribution of U, indicating a combination of AUC and  $UO_2/U_3O_8$ . In some particles, combinations of N and U, believed to be AUC, were found attached to the surface of UO particles.

Particles containing U and F were, on average, much smaller than the average UO particle.



30µm

**Figure 6:** X-ray mapping of UO and AUC particles superimposed on a BS image. Red and yellow pixels symbolize signal from the characteristic X-rays of N and U, respectively. Due to low count rate only the largest particles were registered.

For impactor Stage D at *Site 1*, Bed furnace, uranium aerosols tended to be attached to a non-uranium material consisting predominantly of S, O and probably C. The two lighter areas in Figure 7 correspond to uranium aerosols attached to the material, whose origin still needs to be explained. A corresponding phenomenon was not observed at *Site 4*.



**Figure 7:** A backscatter (left) and secondary electron (right) image of two uranium particles (white) of different size attached to a non-uranium material consisting predominantly of S, O and probably C.

# Discussion

#### **Particle distributions**

The results show that the average uranium aerosol is smaller at *Site 4*, BA grinder than at *Site 1*, Bed furnace. This is not surprising, since the BA pelletizing workshop uses a finer uranium oxide powder than the regular pelletizing workshop. The generally small aerosols at *Site 1* were, however, surprising and are believed to correspond to an AMAD smaller than the ICRP default value of 5  $\mu$ m. This has yet to be confirmed.

Studying Figure 2, it can be observed that there appears to be two 'families' of uranium aerosols - one with very small particles (diameter << 1  $\mu$ m) and one with larger particles. This might be supported by Figure 3, which shows that particle size distribution is not described perfectly by the expected lognormal distribution. The phenomenon is most obvious for impactor Stage A at *Site 1*, Bed furnace. The reason for this has yet to be explained, and explanations other than different 'families' of particles exist. One explanation could be a 'background' of very small particles present at each impaction stage, where particle activity distribution is better explained by the Activity Median Thermodynamic Diameter (AMTD) rather than AMAD. The ICRP states that AMAD is typically applicable to aerosols with AMAD >0.5  $\mu$ m (ICRP 2012). Other explanations could be varying particle density, bias in particle counting due to resolution issues and the fact that the final filter was not analyzed. The phenomenon is much less obvious at *Site 4*, BA grinder. There are two possible explanations for this: 1) There were not as many very small particles or, 2) The SEM image resolution on the MCE filters was worse, due to the non-conducting medium, so that these small particles were not detected.

#### Particle size, shape and chemical form

The INCA software was set so as to register uranium particles only. When a particle was detected, the X-ray spectrum was analyzed, and a list of all elements in the particle presented. The vast majority of uranium aerosols consisted, unsurprisingly, of oxygen apart from uranium. The U/O ratios showed some significant variation, probably due to different combinations of  $UO_2/U_3O_8$  and possibly signal distortion from oxygen in the background support. At *Site 1*, 1-6 % of the uranium aerosols contained fluorine. A quantification of the aerosols containing nitrogen, believed to be AUC, was not possible due to the spectrum analyzing algorithm, which could not identify the weak K<sub>a</sub>-peak of nitrogen. Manual inspection of spectra showed a significant presence of nitrogen in many uranium aerosols. The  $UO_2/U_3O_8$  ratio, UF chemical form and AUC quantification needs further investigation.

For *Site 1*, it was noted for the later impaction stages, especially Stage D, that small uranium particles were obscured by a conglomerate consisting of S, O and probably C. The origin of this material is unclear, but might stem from furnace material or corrosion products from precipitation tanks. The presence of this material made counting of discrete uranium particles difficult due to low contrast of the disturbing material. It is unclear how the uranium particles were incorporated into the material. This is an important observation as it could affect aerosol deposition in the airways, if inhaled, and solubility in body fluids.

The mixture of solid, large aerosols as well as clusters of small  $UO_2$  particles is in agreement with previous studies (Ansoborlo et al., 1997).

#### Impactor cutoffs and AMAD

The particle diameters in Figure 2 are presented as the equivalent particle diameter, which differs from the aerodynamic diameter. Impactor cutoffs are presented in aerodynamic diameters, which can explain the differences between Table 2 and the two sampling sites in Figure 2.

One important output from size distribution and activity measurements is the AMAD, which is required for internal dose estimates. In the present study, observations were made that might add to the uncertainties of AMAD estimates, and hence to dose estimates. For example, it was noted that large particles were frequently capable of reach the later impactor stages (Table 5). It was also noted that large amounts of small particles (<0.2  $\mu$ m) were attached to the early impaction stages, especially at *Site 1*. It still needs to be investigated if the influence on AMAD is significant.

AMAD estimates have yet to be carried out, see Future work below.

#### Uncertainties

Observations were made, that might add to uncertainties in the study:

- In the SEM/EDX scanning procedure, uranium particles are registered based on contrast settings. We experienced a problem with the SEM high voltage supply causing some bias in the image resolution, i.e. we had some problems to detect small particles compared to larger ones, giving a possible bias towards large particles. This is especially true for the later impaction stages for *Site 1*, where particles appeared to be hidden in a foreign material. Bias might also occur if a large particle is viewed as several small ones due to high contrast.
- When random scans using the SEM/EDX equipment were carried out, a particle was required to be completely within the field to be counted. Some particles, especially large ones, were only partially within the field, and would then not be counted.

## Conclusions

The main conclusions of this novel pre-study are:

- Uranium aerosols vary significantly with respect to size and shape. There are indications of different 'families' of particles with respect to size distribution. This was most obvious at *Site 1*, Bed furnace.
- Uranium aerosols are generally observed as discrete particles, but large conglomerates of loosely attached uranium particles were observed at *Site 1*, Bed furnace, as well as *Site 4*, BA grinder.
- Uranium aerosols can consist of mixtures of uranium oxides, fluorides, nitrites and Gd. The aerosols are frequently attached to other elements such as Al and Si in the shape of either discrete particles or other materials.

# **Future work**

Being a pre-study, one aim of the present work was to identify prioritized future studies, including:

- Estimating particle volumes, activities and correlation to the aerodynamic diameter in order to estimate the influence on AMAD calculations,
- Carrying out complete sampling using 8-stage impactors,
- Carrying out radiometric analysis of all impactor stages,
- Additional chemical form analysis, e.g. AUC quantification,  $UO_2/U_3O_8$  ratios, U-F chemical form, and,
- Solubility experiments.

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